

Estimation of the Kinetic Parameters of a Catalytic Cracking Model Case Study

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This paper presents the research regarding determination of kinetic model parameters from a catalytic cracking process. Starting from the Weekman kinetic model, the authors proposed a simplified version of this model and, based on experimental data from a catalytic cracking plant, they have numerically determined the coefficients of the new kinetic model. For this purpose, there were defined two objective functions; the first function is based on errors generated by estimation of the riser outlet temperature and the second function associated to the errors generated by the estimation of the gasoline yield. The minimization of the two objective functions has been solved by using Optimization Toolbox from MATLAB programming language. The results showed that the objective function that depends on gasoline yield allows more accurate estimation of the kinetic parameters from this model.

Keywords: kinetic model, optimization, catalytic cracking

Generally, for a chemical processes and especially for the catalytic cracking process, the kinetic model is responsible for the accuracy of the process model results. These kinetic models are different by pseudo-components number, chemical reactions number and the complexity of the kinetic equations. The number of pseudo-components of the kinetic models is continuously increased in order to obtain a more detailed prediction of products distribution [1]. For example, the first kinetic model proposed by Weekman, it is based on three major pseudo-components: feedstock, gasoline and coke plus light gas [2].

Relevant contributions to improve this kinetic model are presented in following papers [3- 5]. Lee, in the [6] paper, there has dividing the third pseudo-components in two different components in coke and light gasses and obtaining a model with 4-lumps. Anchetya, in his work [7], presents a 5-lump model, considering the coke one pseudo-component and divided the gas in two pseudo-components (liquefied gasses and dry gas).

Hagelberg expanded this model in a 8-lump model by dividing the gasoline fraction into paraffins, olefins, naphthenes and aromatics [8]. For the heavy feedstock's Chiyoda Chemical Engineering and Construction Co. have developed a 6-lump kinetic model, where the feedstock have been divided in two components: residue and heavy gasoil, and the reaction products obtained are: light gasoline, gasoline, gases and coke [9]. Some authors have developed more complex kinetic models, such as 10-lump model [10,11], 12-lump model [13], 13-lump model [14], 19-lump model [15]. These kinetic models are mathematically more complex and they need many coefficients, which are hard to estimate.

Determination of kinetic model coefficients is realised by minimizing an objective function whose structure defined as a sum of errors squared of the selected output variable, deviations calculated based on experimental data and the values determined based on the kinetic model and the reactor model. The process output variable chosen depending on the consistency of experimental data or model sensitivity. The techniques of minimizing the objective function are part for the category of multidimensional optimization algorithms with restrictions [16].

In this context, the authors' researches have oriented to study the coefficients associated with the Weekman kinetic model, following simplification of model and determining the new coefficients.

Weekman kinetic model

The model elaborated for the catalytic cracking processing vacuum distillate; on which starting point are three pseudo-components: A -feedstock; B -gasoline; C- coke + gasses. The kinetic scheme of the Weekman model represented in figure 1 and the chemical reactions occurring in the riser shown in Table 1.

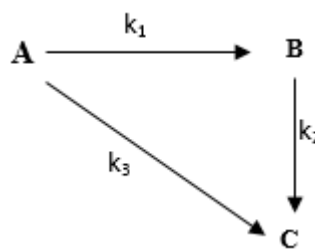


Fig.1. Weekman kinetic scheme

No.	Reaction	Reaction velocity $\left[\frac{kg_{product}}{kg_{react} \times s} \right]$	Activation energy [kcal/mol]
1	A \longrightarrow B	r_1	10000
2	B \longrightarrow C	r_2	18000
3	A \longrightarrow C	r_3	10000

Table 1
CHEMICAL REACTIONS IN WEEKMAN
KINETIC MODEL

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The following relations express the third velocity reactions from Weekman kinetic scheme:

$$r_1 = -k_1 * Y_A^2 \quad (1)$$

$$r_2 = -k_2 * Y_B \quad (2)$$

$$r_3 = -k_3 * Y_A^2 \quad (3)$$

where:

k_1, k_2, k_3 - velocity reaction constants, $\left[\frac{kg_{product}}{kg_{react} \times s} \right]$;

Y_A - weight fraction of the feedstock in the reaction average;

Y_B - weight fraction of gasoline in the reaction average;

Y_C - weight fraction of gas and coke in the reaction average.

The velocity reaction constants k_1, k_2, k_3 are dependent on the feedstock composition, riser temperature, equilibrium catalyst activity and the process operating conditions. These velocity reaction constants can be calculated based on Wollaston's relation [17]:

$$k_j = k_j^0 \cdot f_j(MAT) \cdot \theta_j(t_c) \cdot \gamma_j(c_{coke}) \cdot e^{\left(\frac{E_j}{R} \right) \left(\frac{1}{T_0} - \frac{1}{T} \right)}, \quad j = 1, \dots, 3, \quad (4)$$

where k_j^0 is velocity reaction constant of the at 482°C, expressed in s^{-1} .

The rest of elements of the equation (4) have the following meanings [4, 18]:

$f_j(MAT)$ - attenuation function, that takes in consideration the effect of the equilibrium catalyst's activity;

$\theta_j(t_c)$ - attenuation function, that takes in consideration the effect of the coke catalyst's deactivation;

$\gamma_j(c_{coke})$ - attenuation function, that takes in consideration the effect of the residual coke;

E_j - activation energy of the chemical reaction, $\left[\frac{kcal}{mol} \right]$;

T - current riser temperature, [K];

T_0 - set point temperature, [K];

R - universal gas constant, $\left[\frac{m^3 \cdot atm}{kmol \cdot K} \right]$.

The reactor model of the catalytic cracking

The catalytic cracking reactor is a system with distributed parameters; authors in the paper [4, 18] have presented the model. The model contains a differential equations system, based on material and heat balance.

$$\begin{cases} \frac{dY_A}{dz} = -\frac{1}{U_v} (k_1 + k_3) Y_A^2 \\ \frac{dY_B}{dz} = \frac{1}{U_v} (k_1 Y_A^2 - k_2 Y_B) \\ \frac{dY_C}{dz} = \frac{1}{U_v} (k_2 Y_B + k_3 Y_A^2) \\ \frac{dT_r}{dz} = \left(-\frac{dY_A}{dz} \right) * \frac{(-\Delta H_{r1})}{(Y_A c_{pA} + R_{abur} c_{pabur} + R_{cat} c_{pcat})} \end{cases} \quad (5)$$

The initial conditions used to solve the differential equations system (5) are:

$$\begin{cases} Y_A(0) = 1 \\ Y_B(0) = 0 \\ Y_C(0) = 0 \\ T(0) = T_{nod} \end{cases} \quad (6)$$

The significance of the measures used in the model is the following:

U_v - riser vapours velocity expressed by relationship

$$U_v = \frac{1}{3600} * \frac{Q_{mp}}{\rho_v * A_r * E}; \quad (7)$$

Q_{mp} - feedstock flow $\left[\frac{kg}{h} \right]$;

A_r - the cross-sectional area of the riser [m^2];

ρ_v - density in vapour phase inside riser $\left[\frac{kg}{m^3} \right]$;

E - volume fraction of the catalysts;

ΔH_{r1} - enthalpy of the first reaction $\left[\frac{kcal}{kg_{comp. reac.}} \right]$;

Q_A, Q_B, Q_C - pseudo-component weight rate $\left[\frac{kg}{h} \right]$;

Q_{cat} - catalyst weight flow $\left[\frac{kg}{h} \right]$;

Q_{abur} - steam weight flow $\left[\frac{kg}{h} \right]$.

Simplifying the kinetic model Weekman and objective function development

Starting from kinetic model Weekman completed with Wollaston's relationships, the authors simplified velocity constants expressions and proposing following relations

$$k_j = k_j^0 e^{\left(\frac{E_j}{R} \right) \left(\frac{1}{T_0} - \frac{1}{T} \right)}, \quad j = 1, \dots, 3 \quad (8)$$

in which we have the following variable:

E_j - activation energy of reaction, $\left[\frac{kcal}{mol} \right]$;

T - current riser temperature, [K];

T_0 - set point temperature, [T];

R - universal gas constant, $\left[\frac{m^3 \cdot atm}{kmol \cdot K} \right]$.

In the kinetic relation (1-3), the activation energy has values taken from literature, Table 1 [19]. Giving up of Wollaston's relations implies the recalculation of velocity constant $k_j^0, j=1, \dots, 3$ from experimental date. In Table 2 are represented the experimental data that are used to recalculate the velocity constant of the reaction at 482°C.

Determination of the velocity constants $k_j^0, j=1, \dots, 3$ related to reaction velocity are realized by minimization the following objective function

$$f_{ob}(k_1^0, k_2^0, k_3^0) = \sum_{j=1}^m [T_j^{exp} - T_j^{calc}(k_1^0, k_2^0, k_3^0)]^2 \quad (9)$$

where T_j^{exp} represents the experimental riser temperature; $T_j^{\text{cal}}(k_1^0, k_2^0, k_3^0)$ - the temperature calculated with reactor model, for the same values of input data from experimental set j .

For the transformation reaction of the feedstock in gas and coke, the special literature indicates the value $k_3^0 = 0.05 \text{ s}^{-1}$, value adopted by the authors. In this condition, the objective function (9) is

$$f_{ob}(k_1^0, k_2^0) = \sum_{j=1}^m [T_j^{\text{exp}} - T_j^{\text{cal}}(k_1^0, k_2^0)]^2 \quad (10)$$

Considering the multivariable character of the function (10) and the structure of mathematical model of the reactor (5), the determination of a function minim can be done using algorithm, dedicated for the nonlinear function.

Programming the optimization problem

The optimization problem was solved using the MATLAB programming environment. In this environment, the Optimization Tool is used, respectively `fmincon` routine, figure 2. This routine is dedicated to calculate the optimum point for nonlinear multivariable functions under nonlinear restrictions. The objective function is programmed in the *riser_optim* module, the initial solution chosen for values

$\begin{bmatrix} 1 \\ 0.5 \end{bmatrix}$ and the interval of research for each of both variables

of function (10) is $\begin{bmatrix} 0 \\ 2 \end{bmatrix}$.

Table 2
EXPERIMENTAL DATA FROM CATALYTIC CRACKING PLANT

Feedstock property					Operated data					
Day	Density	Sulphur [% mass]	Boiling temperature at 10% volume [° C]	Boiling point medium temperature [° C]	Feedstock temperature [° C]	Feedstock flow [kg/h]	Regenerator temperature [° C]	Catalyst rate	Reactor temperature [° C]	Gasoline flow [kg/h]
1	0.912	0.40	299	378	203	176292	711	4.67	531	75417
2	0.914	0.40	286	370	200	177083	710	4.36	531	82917
5	0.907	0.35	263	364	207	155667	706	4.68	530	69375
6	0.907	0.32	262	365	205	161083	708	4.56	530	75583
8	0.908	0.37	284	367	194	157792	711	4.63	531	71167
9	0.911	0.35	275	367	195	161750	709	4.59	531	74167
12	0.907	0.32	281	366	191	169542	711	4.54	532	78333
13	0.906	0.33	282	370	198	170375	710	4.49	531	80208
14	0.906	0.34	280	363	205	173167	710	4.57	531	80417
15	0.910	0.36	287	368	205	167333	712	4.48	531	79300

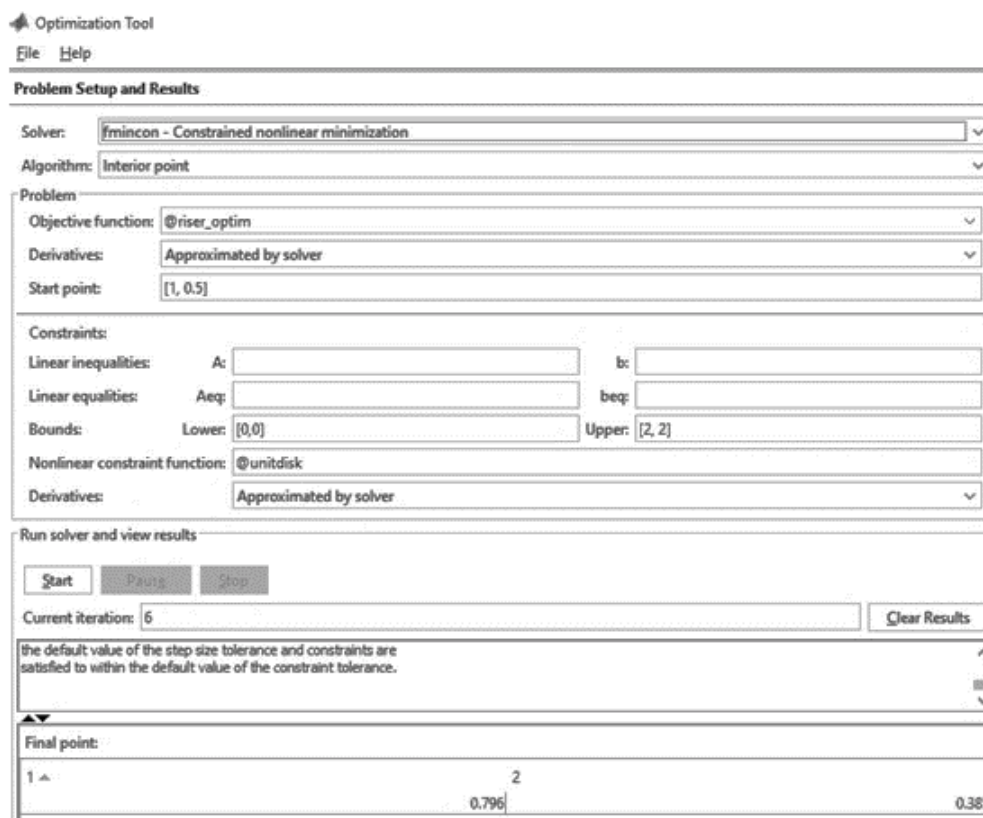


Fig. 2. Interface Optimization Tool

The implementation of the objective function in MATLAB has raised programming problems due to language specificity respectively a reduced possibility of the data transfer between the program modules. The objective function module is implemented as a *riser_optim* function

function S = riser_optim(x)

where x variable represents the vector which contains the values of velocity reaction constant at 482°C, respectively k_j^0 ; S - the value of the objective function (10).

In this programming mode, the function can be subordinated to optimization module because the function variables are the independent variables by the optimizer module. In order to be able to calculate the deviation square sum from relation (10), it was defined an iterative structure with m iteration, which can realize the following operations:

a) Download into the reactor model variables the experimental input data associated to experiment j ;

b) Calculate using heat balance the value of the mixing node temperature. This temperature represents one of the initial conditions of a differential equation system associate to the catalytic cracking reactor;

c) Integration of differential equation system using *ode23s* function. This function gives back the results calculated by integrating differential equations system as matrix of $[z, y]$, where z is the vector associated with to current point from riser, and y contains several numbers of vectors associated to integrated variable;

d) The calculation of the squared deviation of the riser temperature and the summing of deviations defined in relation (10).

The mathematical model of catalytic cracking reactor contains the kinetic model and material mass balance and heat balance equations. The reactor model is implemented in MATLAB by a multivariable function:

function dydz=f(z,y,u,k0)

where the variables are:

dy/dz - vector that contains the value of the mathematical model derivatives;

z - current position;

y - vector that contains components concentration;

u - vector that contains the values of the input experimental model measurements;

k_0 - reaction velocity constants vector at 482°C k_j^0 .

Results and discussions

Running the optimization programme there were followed three objectives: testing optimizer algorithm stability, the influence of the initial solution and the determination of simplified Weekman model coefficients.

The numerically tests show a strong relation between algorithm stability and initial solution. For some initializations solutions values we get optimal values between a short range and the objective function is almost constant. In *figure 3* it is represented the action module of the optimization programme, and the conclusion is that the optimization algorithm is faster closing to the optimum point and after this step followed by a slowly movement to it.

This evolution is demonstrating the fact that the objective function is characterized by a plateau evolution around the optimum point.

The optimization algorithm performance was study by the behaviour of the objective function near the optimal point, *figure 4*. The conclusion is that the function minim is not too well defined; reversed banana evolution is much more relevant.

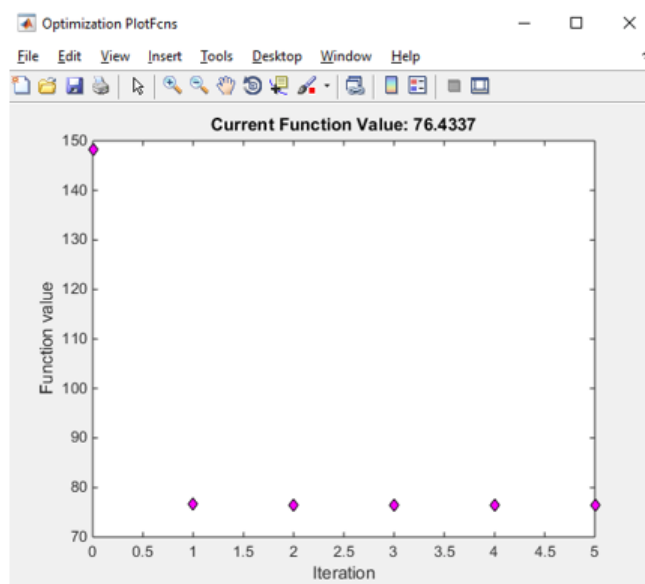


Fig. 3. Objective function values evolution

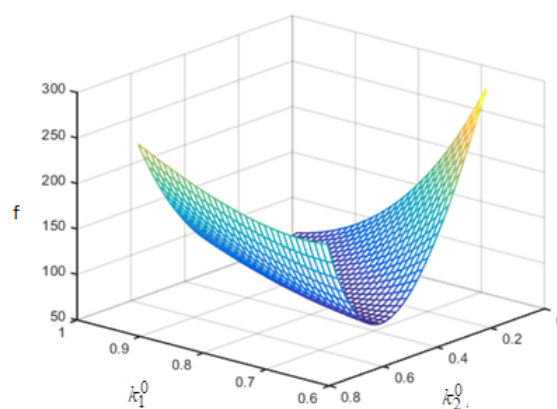


Fig. 4. Objective function graphic representation

Analysis of contour curves associated to objective function, *figure 5*, validates the previously formulated hypothesis. It is found that these contour curves are extremely elongated confirms the reverted banana aspect of the objective function. In these conditions, the determination of the optimum point can be extremely difficult.

Another conclusion resulting from this analysis was the need to reduce the initialization interval of the solutions (searching interval). Looking on equation (10), objective function has the T^2 signification. At an average of 76 and for 15 experimental points, the resulted average deviation

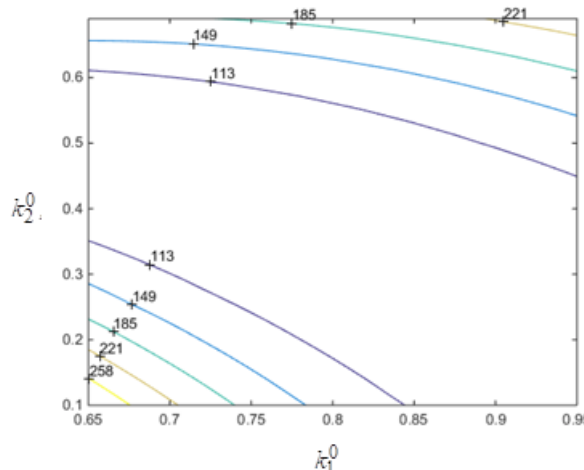


Fig. 5. Contour curves of objective function

	X0		Xopt		Fob
Group 1	0.65	0.10	0.96	0.18	76.36
	0.70	0.19	0.99	0.20	79.75
Group 2	0.75	0.29	0.79	0.35	77.79
	0.80	0.39	0.80	0.37	76.44
Group 3	0.65	0.29	0.74	0.41	76.93
	0.65	0.60	0.84	0.36	76.93

Table 3
THE RESULTS OBTAINED DURING PROCESS
OPTIMIZATION RESULTS

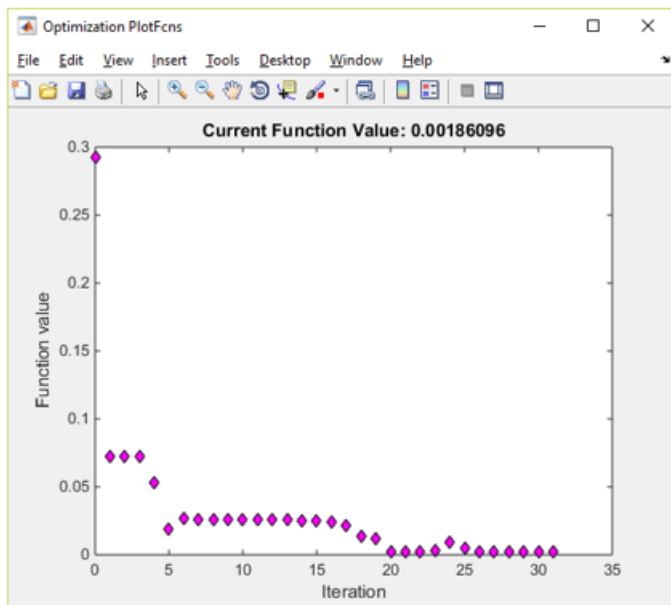


Fig. 6. Evolution of the objective function value to minimize the function (11)

of 2.25 °C is obtained, the accepted value for the estimated kinetic purposed constants for Weekman kinetic model. Table 3 contains some of the obtained results from already run optimizing tests.

The results can be grouped in three categories based on the optimum solution value. It is noticed that the optimum solution values are different, and more for the second variable, k_2^0 .

The high value of the objective function suggests that the temperature at the riser outlet is not suitable for determining the coefficients of the kinetic model. In support of this statement, the authors indicate that the temperature measured in the riser is in fact a controlled temperature and implicitly its value is not sensitive to the input variables of the mathematical model of the process. In this case, the authors investigated the possibility of using another objective function, which would allow for the determination of coefficients of the kinetic model with better precision.

Because the experimental database contains information about the feed rate and gasoline flow obtained, and assuming the plant is stationary without mass accumulation regimes, the gasoline yield is given by the ratio of the two flows. In these conditions, the objective function (10) becomes:

$$f_{ob}(k_1^0, k_2^0) = \sum_{j=1}^m [\eta_j^{exp} - \eta_j^{calc}(k_1^0, k_2^0)]^2 \quad (11)$$

Minimizing the objective function (11) was performed using the same MATLAB function, respectively fmincon. The initial values of the optimum point were considered [0.5; 0.5] and the optimum interval for this researcher $k_1^0 \in [0.1...2]$ and $k_2^0 \in [0.1...2]$.

Figure 6 shows the evolution of the objective function value during the iterations. It is observed that after the first

Table 4
INFLUENCE OF THE INITIAL SOLUTION ON STABILITY AND
OPTIMAL SOLUTION

X0		Xopt		Fob
1.0	1.00	1.45	0.970	0.00190
2.0	0.50	1.54	1.000	0.00185
1.2	0.65	1.35	0.924	0.00187
1.4	0.75	1.45	0.979	0.00186
1.6	0.85	1.51	1.020	0.00180
1.8	0.95	1.47	0.960	0.00186

5 iterations, the optimal function evolves to a plateau, the function value slowly decreasing or remaining constant. Iterations 20 ... 30 highlight the near-constant evolution of the value of the objective function.

The stability of the optimization algorithm is tested by running the program for different initial values of the optimal solution and the values in Table 4 are eloquent in this respect.

In these conditions, the authors believe the optimization algorithm has determined the optimal solution $k_1^0 = 1.43$ and $k_2^0 = 0.79$.

The graphical representation of function (11), Figure 7, highlights the existence of a tolerable range of variables k_1^0 and k_2^0 , a domain which is bounded by a wall of the objective function (11), a wall that reflects a large and abrupt increase in the value of the objective function.

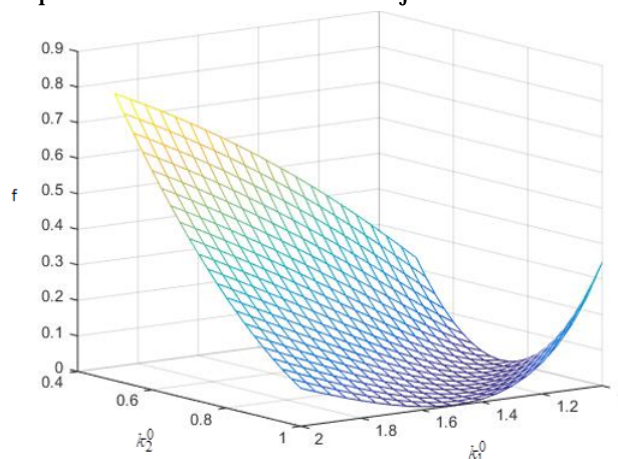


Fig. 7. 3D representation of an objective function (11).

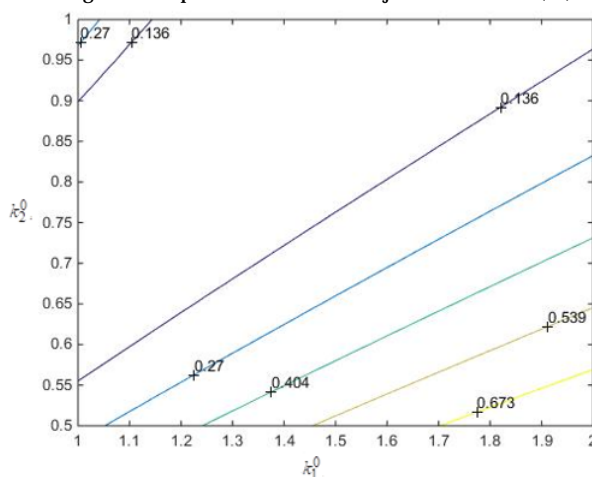


Fig. 8. Function (11) surface protection in plan k_1^0, k_2^0

The interior of the domain leads to a similar area with the graphical representation of the function Rosenbrooke, respectively the banana function [20]. The analysis performed demonstrates that the choice of the initial solution is decisive for the stability of the algorithm.

Figure 8, projection of the response surface on the plane k_1°, O, k_2° , represents a new argument to sustain what was said before. It is noticed that the feasibility zone of the minimum function (11) is a strip bounded by the lens function wall.

Conclusions

In this paper, numerical aspects regarding the estimation of the parameters of the Weekman kinetic model, simplified model of authors, are treated with experimental data from a catalytic cracking industrial plant. The main contributions of the authors are as follows:

- Elaboration of two objective functions, one related to the errors generated by the estimation of the outlet temperature from the riser and the second one associated to the errors generated by the estimation of the gasoline efficiency;

- Minimizing these functions was done using the Optimization Tool from MATLAB programming language;

- A plate around the optimum point characterizes the objective function associated with errors generated by the estimation of the outlet temperature. In these conditions, the minimum of this is not very well defined and the estimation of the kinetic model parameters is difficult.

- The objective function associated with the errors generated by the estimation of the gasoline yield has a graphical representation, which indicates an area of existence of the banana end, which defines a tolerable range for model parameters much better than the one associated with the first objective function. Using this function, the constants of the proposed kinetic model were calculated.

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